Application Serial No.: 10/522,826 Attorney Ref: 63619.US / 6710.0.Germany Client Ref: LGFILGRASTIM

(LB/G-32991A/LEK)

AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions and listings of claims in the application:

Listing of Claims:

 (Currently Amended) A process for the production of a biologically active protein <u>selected</u> from the group consisting of G-CSF, GM-CSF, M-CSF, EGF, HAS, DNAse, FGF, TNF-alpha, TNF-beta, interferons, and interleukins, comprising:

expressing said protein as a heterologous protein in an expression system comprising a cultivated organism having <u>at least</u> one <u>cell or more cells</u>, wherein the protein is expressed as a substantially correctly folded protein precursor, <u>wherein the protein precursor has an aqueous solubility</u>, in <u>non-classical</u> inclusion bodies having an aqueous solubility in the cells of the organism;

regulating one or more cultivation parameters selected from the group consisting of temperature of cultivation, composition of cultivation medium, induction mode, principle of performing the fermentation, addition of a stress induction agent an agent eapable of causing stress, and co-expression of auxiliary proteins, wherein regulating the one or more parameters increases the proportion of substantially correctly folded protein precursor present in the non-classical inclusion bodies in the cell[[s]], relative to the proportion of substantially correctly folded protein precursor present in inclusion bodies in a cell[[s]] of an organism not cultivated by regulating said parameters;

isolating the non-classical inclusion bodies from the cell[[s]] of the organism;

optionally, washing the non-classical inclusion bodies;

solubilizing the substantially correctly folded protein precursor from the <u>non-classical</u> inclusion bodies under non-denaturing conditions <u>by contacting the non-classical inclusion bodies</u> with a <u>non-denaturing aqueous solvent having a pH of about 8.0</u>; and

purifying the biologically active protein from the solubilized substantially correctly folded protein precursor and non-denaturing aqueous solvent,

wherein the process for the production of the biologically active protein is free from any denaturation and renaturation of the protein.

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(Canceled).

(Cancelled).

 $4. (Previously \ Presented) \ A \ process \ for the \ production \ of a \ protein \ according \ to \ claim \ 1, wherein \ the$

selected heterologous protein is G-CSF.

5. (Previously Presented) A process for the production of a protein according to claim 1, wherein the

cultivated organism is selected from the group consisting of bacteria and yeasts.

6. (Previously Presented) A process for the production of a protein according to claim 5, wherein the

cultivated organism is the bacterium E. coli.

7. (Previously Presented) A process for the production of a protein according to claim 1, wherein the

heterologous protein is accumulated in the inclusion bodies to a proportion of at least about 10%,

relative to the total protein mass of a cell of the organism used in the expression system.

8. (Canceled).

9. (Canceled).

10. (Previously Presented) A process according to claim 1, wherein the temperature of cultivation

ranges from about 20° C to about 30° C.

11. (Canceled).

12. (Previously Presented) A process according to claim 1, wherein regulating the induction mode

comprises selecting an inducer from the group consisting of IPTG, lactose, and NaCl.

13. (Previously Presented) A process according to claim 12, wherein the selected inducer is IPTG.

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14. (Previously Presented) A process according to claim 13, wherein the concentration of IPTG

ranges from about 0.1 mM to about 1 mM.

15, (Previously Presented) A process according to claim 14, wherein the concentration of IPTG is

about 0.4 mM

16. (Previously Presented) A process according to claim 12, wherein the regulation of the induction

mode further comprises adding the inducer at the beginning of the fermentation.

17. (Previously Presented) A process according to claim 1, wherein the principle of performing the

fermentation is selected from the group consisting of performing of fermentation in a batch

mode, performing of fermentation in a fed batch mode and performing of fermentation in one or

more shake flasks.

18. (Canceled).

19. (Previously Presented) A process according to claim 1, wherein the composition of the

cultivation medium is selected from the group consisting of GYST, GYSP, LYSP, LYST,

LBON and GYSPON.

(Previously Presented) A process according to claim 19, wherein the selected medium is GYST;

or GYSP.

21. (Currently Amended) A process according to claim 1, wherein the stress induction agent agent

additive which is capable of causing stress is selected from the group consisting of ethanol and

propanol.

22. (Canceled).

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23. (Previously Presented) A process according to claim 1, wherein the step of washing comprises contacting the inclusion bodies with a solution selected from the groun consisting of Tris/HCI

buffer, phosphate buffer, acetate buffer, citrate buffer and water.

24. (Previously Presented) A process according to claim 23, wherein the concentration of the

selected buffer ranges from about 1 mM to about 10 mM.

25. (Previously Presented) A process according to claim 23, wherein the selected solution is water.

26. (Currently Amended) A process for production of a protein according to claim 1, wherein the

step of solubilizing the substantially correctly folded protein precursor from the inclusion bodies further comprises contacting the inclusion bodies with non-denaturing acucous solvent

solution is selected from the group consisting of aqueous solutions of: urea ranging in

solution is selected from the group consisting of aqueous solutions of: urea ranging in concentration from about 1M to about 2M, N-lauroyl sarcosine ranging in concentration from

concentration from about 1M to about 2M, N-lauroyl sarcosine ranging in concentration from about 0.05% to about 0.25% mass per volume, betain, sarcosine, carbamoyl sarcosine, taurine, DMSO, non-detergent sulfobetains, and a buffer in a high, solubilising concentration, said buffer

being selected from the group consisting of HEPES, HEPPS, MES, and ACES.

27-37. (Canceled).

38. (Currently Amended) The process of claim 26, wherein the non-denaturing aqueous solvent

 $\underline{solution \ is} \ \underline{comprises} \ \underline{a} \ \underline{relatively} \ \underline{low} \ \underline{concentration} \ \underline{of} \ N\text{-lauroyl sarcosine} \ \underline{in} \ \underline{water, in} \ \underline{order} \ \underline{to}$

avoid denaturing conditions.

39. (Previously Presented) The process of claim 38, wherein the concentration of N-lauroyl

sarcosine further ranges from about 0.1% to about 0.25% mass per volume.

40. (New) The process of claim 4, wherein the specific activity of the G-CSF is at least 1x107

IU/mg.

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- 41. (New) The process of claim 1, wherein the amount of protein expressed is at least about 20% by mass of the total mass of proteins produced by the host cell.
- 42. (New) The process of claim 1, wherein the amount of protein expressed is at least about 30% by mass of the total mass of proteins produced by the host cell.